

# Oxyfuel combustion has come a long way, but.....

**IEAGHG 2nd Oxyfuel Conference 2011**

11<sup>th</sup> – 16th of Sept 2011

**Yeppoon QD, Australia**

**Lars Strömberg**

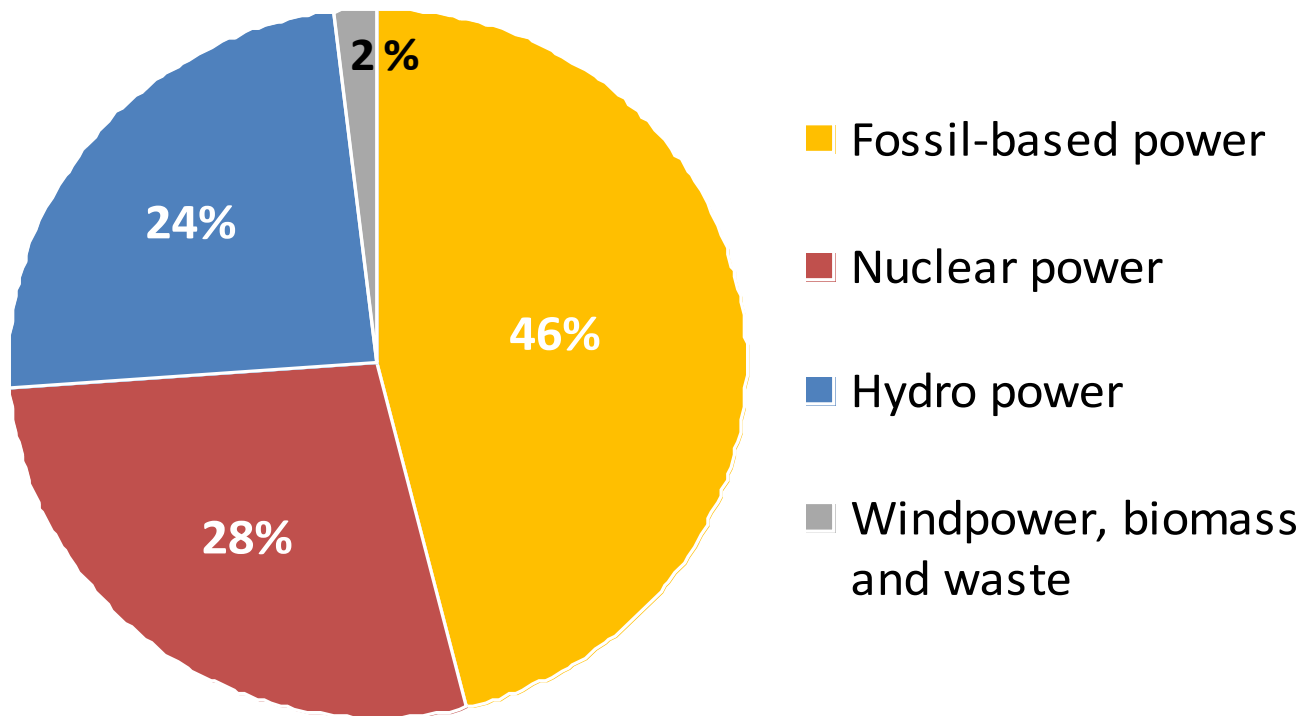
**Vattenfall AB**

# Vattenfall – A leading European energy company

- 200 TWh electricity - nuclear, hydro, coal, gas, wind
- 40 TWh heat – biomass, coal gas
- 40 000 employees
- 90 million tons of CO<sub>2</sub>



# Generation portfolio totalling about 40,000 MW



\* Vattenfall has 1200 MW installed capacity from wind and 600 MW under construction.

# CCS - Roadmap to realisation

## Conceptual investigations

### Experimental Research

0.1 – 0.5 MW<sub>th</sub>  
< €10 million



### Pilot plant

30 MW<sub>th</sub>  
€100 million



### Demonstration plant

300 – 700 MW<sub>th</sub>  
~ €1000 million



### Commercial concept:

~ 1000 MW<sub>th</sub>



1999

- Theoretical studies

2002

- Research
- Basic principles
- Combustion characteristics

2008

- Demonstration of the process chain
- Interaction of components
- Validation of basic principles and scale-up criteria
- Long term characteristics
- Non-commercial

2013 – 2015

- Verification and optimization of the component choice, the process and reduction of risks
- Must be commercially viable incl. subsidies

2020

- Competitive on the market at that time
- No subsidies



# View on Oxyfuel Pilot Plant





# Results until May 2011

<b>Operating hours</b>	<b>14.200</b>
<b>Captured amount of CO<sub>2</sub></b>	<b>11.500 t</b>
<b>CO<sub>2</sub>- removal rate</b>	<b>&gt; 93 %</b>
<b>CO<sub>2</sub>- purity</b>	<b>&gt; 99.7 %</b>

- 
- Stable oxyfuel operation
- All emission and safety values contained
- Interaction between all plant components and subsystems validated
- Over 50 tests with Boiler, ASU, CO<sub>2</sub> plant and all other components
- Plant availability very high
- Integration of a "cold DeNO<sub>x</sub>"

**4 different burners tested**

**New tail end concepts commissioned with good results**



## Burning coal in the pilot plant

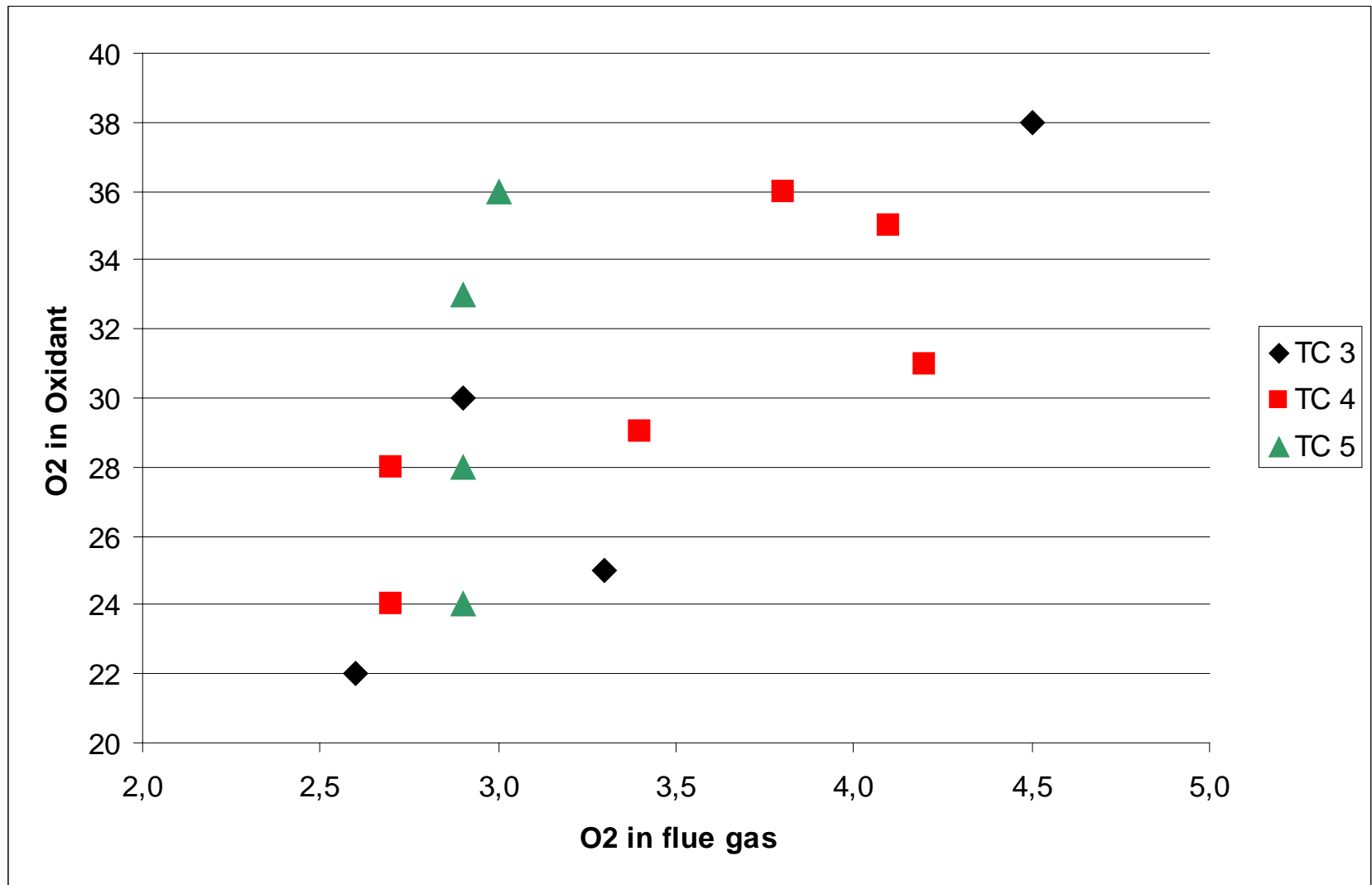


# One of the oxyfuel burners



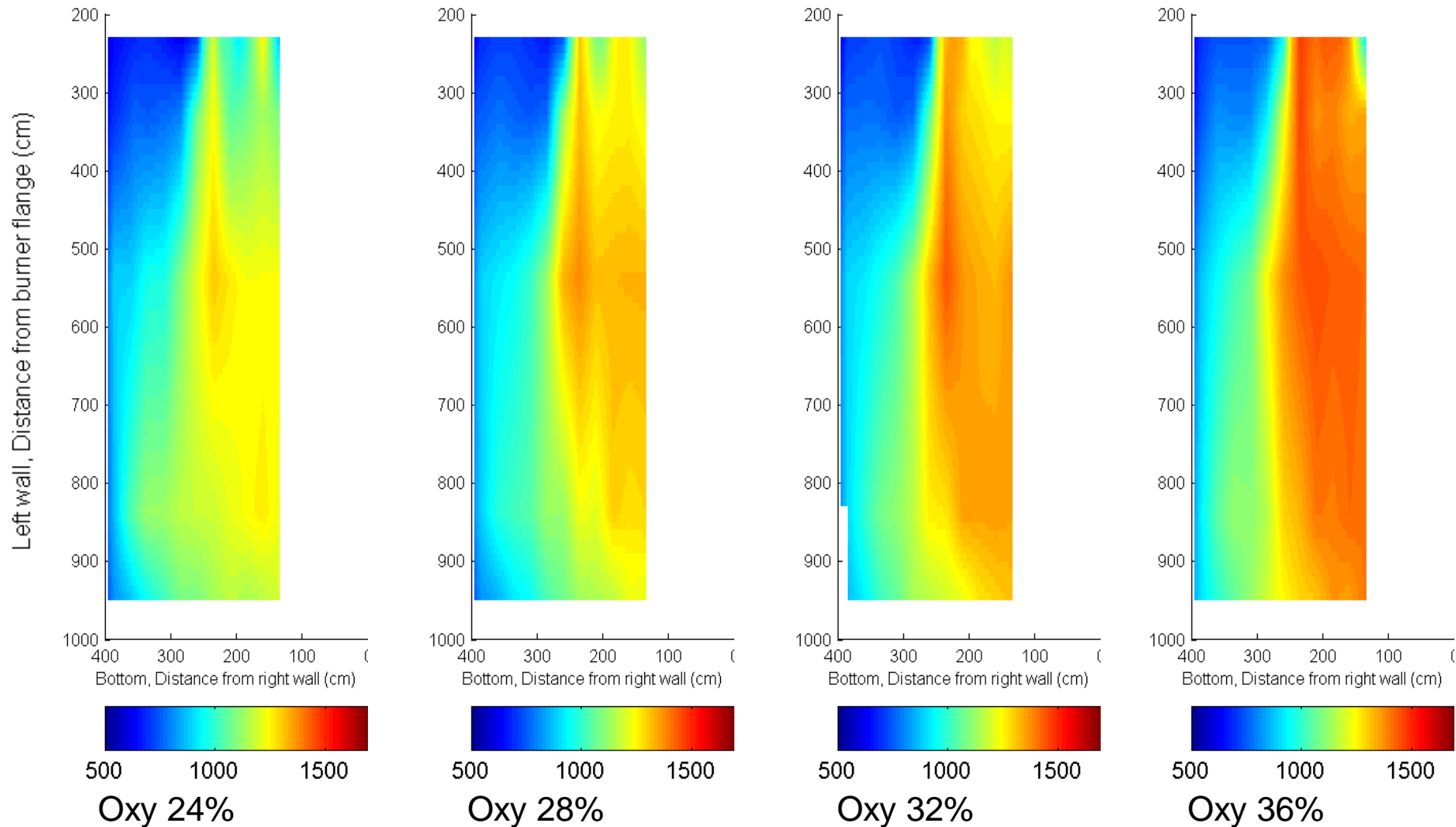


## A wide operational envelope – Some experimental settings with one of the burners

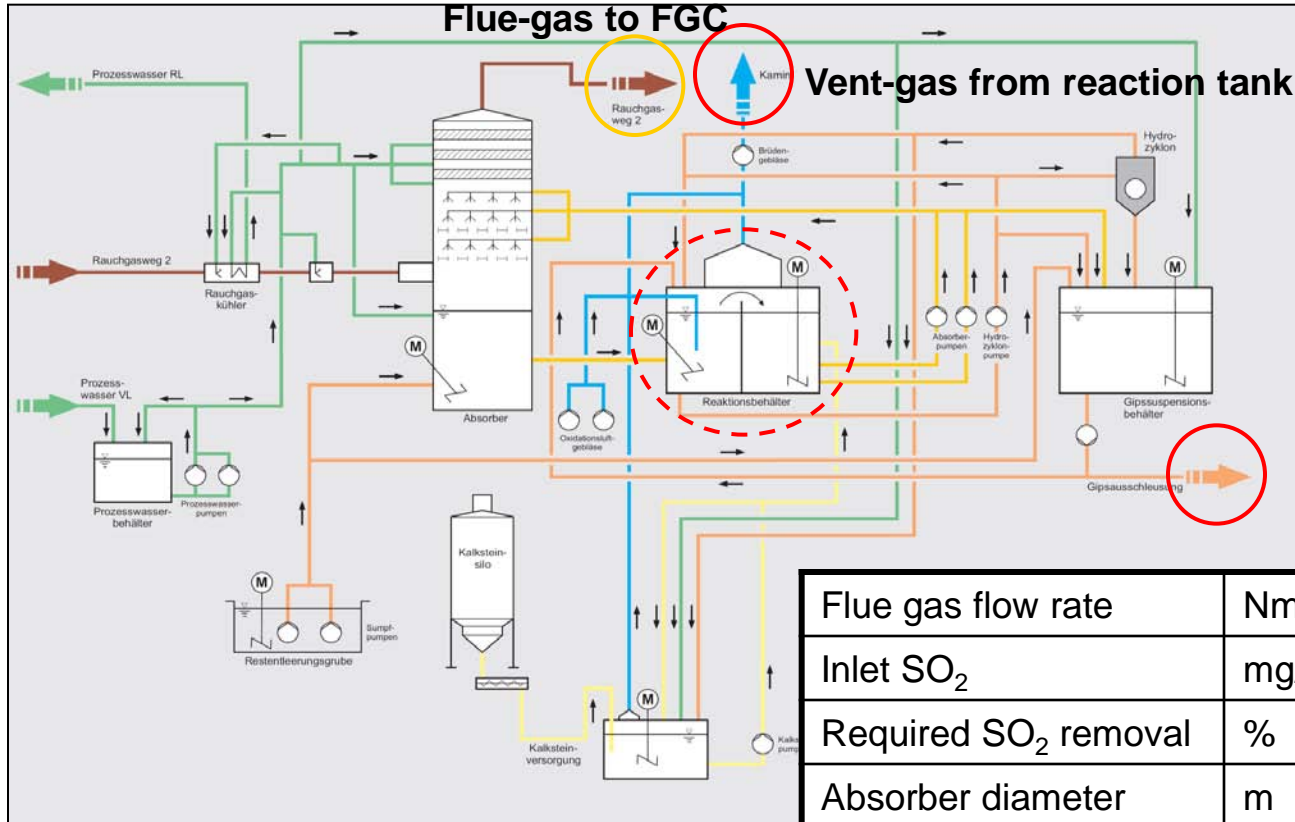


# Temperature Comparison (FTIR)

## Front View



# FGD System – Flow Diagram



Tray absorber (3 trays)  
Three spray levels

External oxidation  
• new emission stream

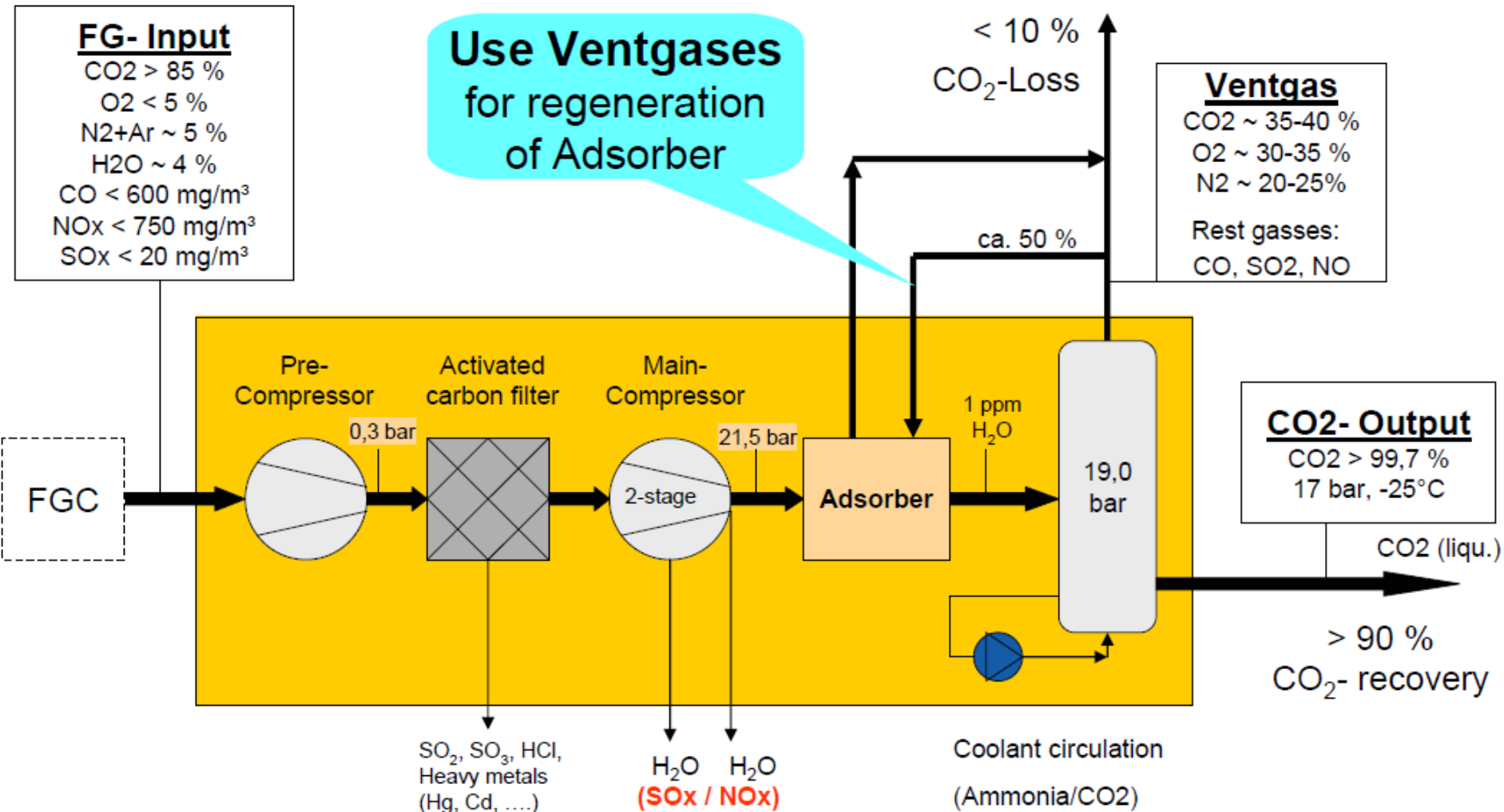
Flue gas flow rate	Nm <sup>3</sup> /h wet	12,000
Inlet SO <sub>2</sub>	mg/Nm <sup>3</sup> , dry	11,500
Required SO <sub>2</sub> removal	%	99
Absorber diameter	m	1.3
Absorber height	m	16.5
Total slurry volume	m <sup>3</sup>	60

# FGC System



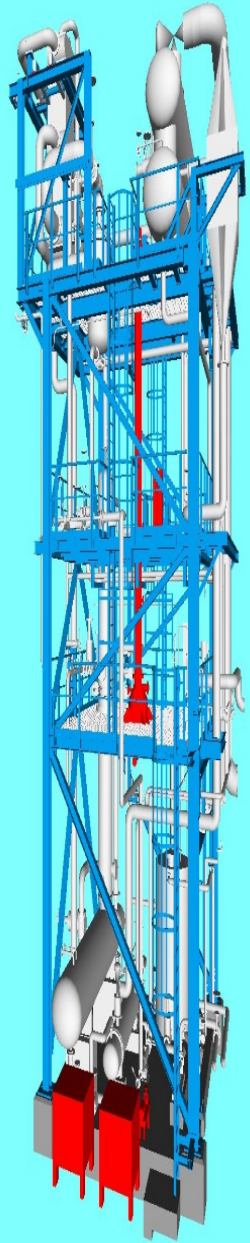
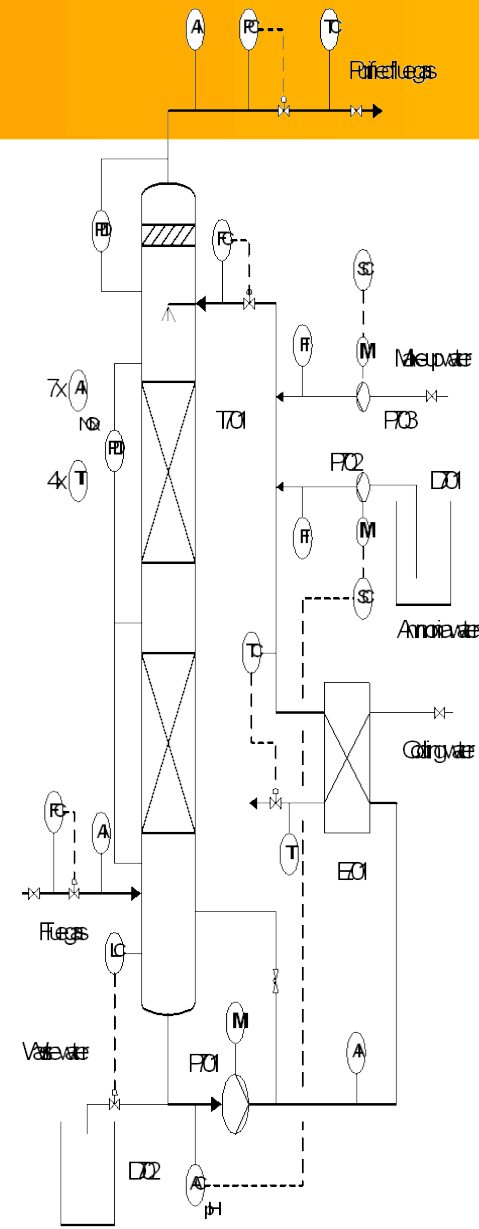


# Overview Pilot Plant Gas Processing Unit (GPU)



# Linde's Alkali Washing Pilot

Absorption of  $\text{NO}_x$  in ammonia -  
Under pressurised conditions  
through a scrubber



## Characterisation and Evaluation of new technology for CO<sub>2</sub>- processing

- Integrated flue gas treatment,
  - CO<sub>2</sub>-separation
  - Membrane unit
- 
- ▶ Technology proved in laboratory scale, now validated
  - ▶ Specific energy demand reduced 30 – 50 %/t CO<sub>2</sub> sep.

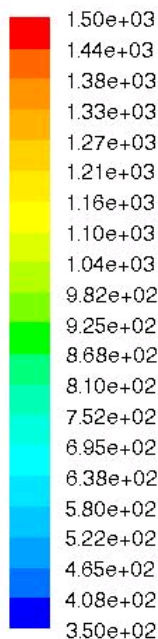
### Budget

10 Mio € Capital Costs

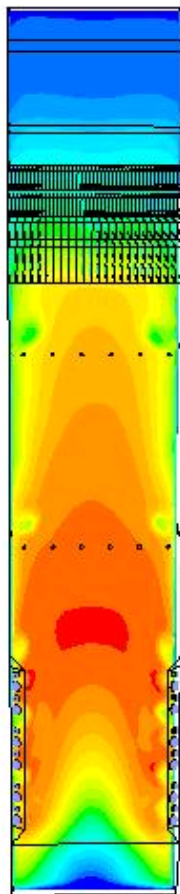
1,6 Mio € R&D Costs



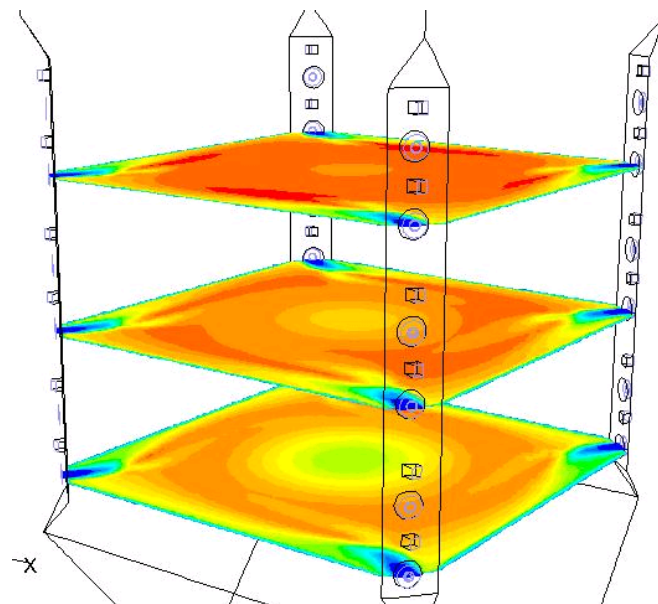
# Modelling of CO<sub>2</sub> Capture process options



Scale in °C,  
red indicates  
1500°C or  
more, dark  
blue indicates  
350°C or less



Temperature profile in a cross section through the centre of the furnace.



Temperature in three horizontal cross sections through the burner rows 1, 3 and 5 counted from the bottom of the furnace.



# Material testing, corrosion characterisation

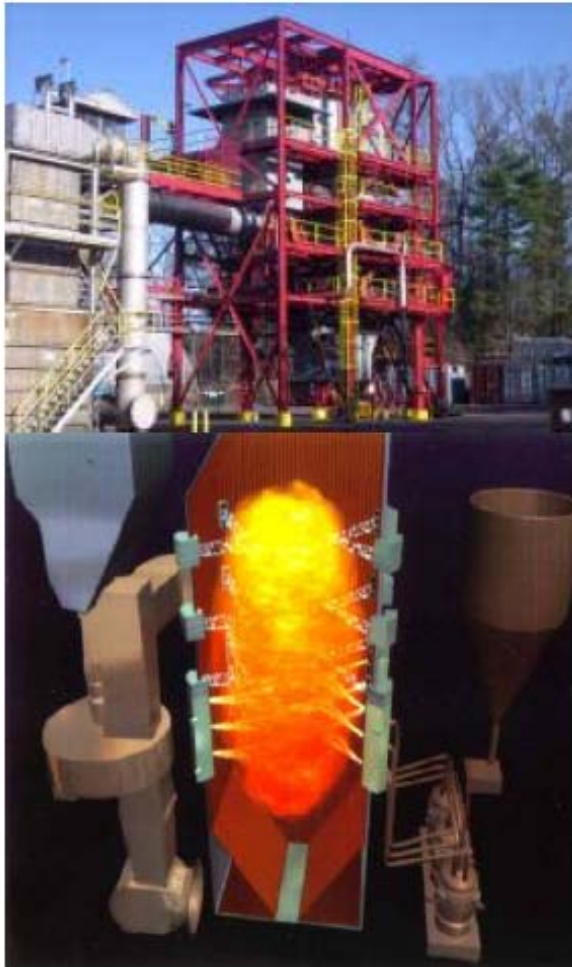
- Testing of common materials used in power plants and some materials under development long time, varying conditions
  - Superheaters, economisers, water walls, ducts, FGD and FGC
  - CO<sub>2</sub> compression (impeller, intercoolers)
- Probe testing and on-line corrosion sensors
  - Cooled and uncooled material probes
  - Metallographic investigations, deposit analysis



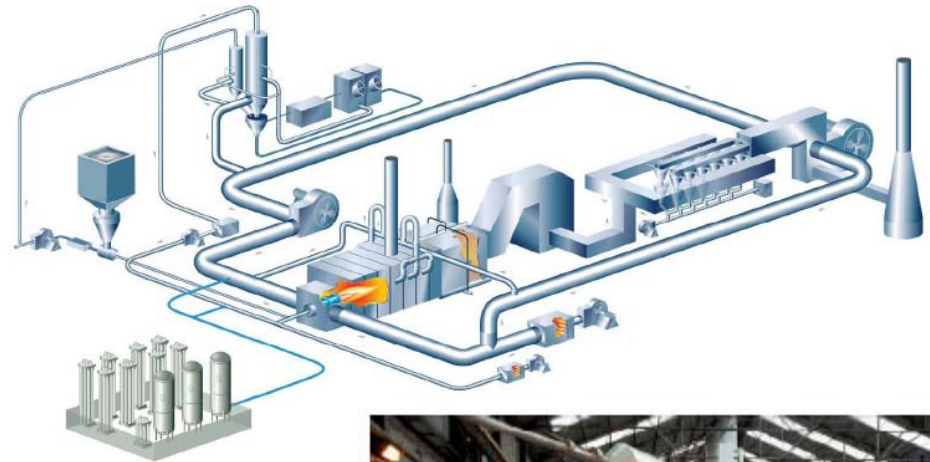
# Alstom T-firing and OxyCoal UK2 projects

## Burner and firing concept testing in 30-40 MW<sub>th</sub> scale

### Alstom Boiler Simulation Facility



During Summer 2009, Doosan Babcock Energy has commenced its 40MW<sub>t</sub> OxyCoal™ demonstration, the world's largest demonstration of an oxyfuel combustion system.



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# Overall Conclusions

- The Oxyfuel Pilot Plant operates better than expected and capture rate, CO<sub>2</sub> quality, effluent stream characteristics and emission standards are all better than expected.
- No show stoppers have been identified
- The standard boiler works excellent, with a large flexibility
- The standard ESP performs better in oxyfuel mode.
- The standard desulphurization unit works better in oxyfuel mode
- The standard flue gas condensation unit is efficient and well performing
- The gas processing unit performs very well and several design options have been identified
- Alternative technologies for gas processing are tested successfully
- A demonstration plant can be built using standard components with standard chemical engineering and power plant knowledge
- We have filed an application to the EU under the NER 300 program, for a demo based on this experience.

# The Costs of CO<sub>2</sub> Capture, Transport and Storage

March 2<sup>nd</sup>, 2011

Lars Strömberg



# European Technology Platform for Zero Emission Fossil Fuel Power Plants



## ETP Role:

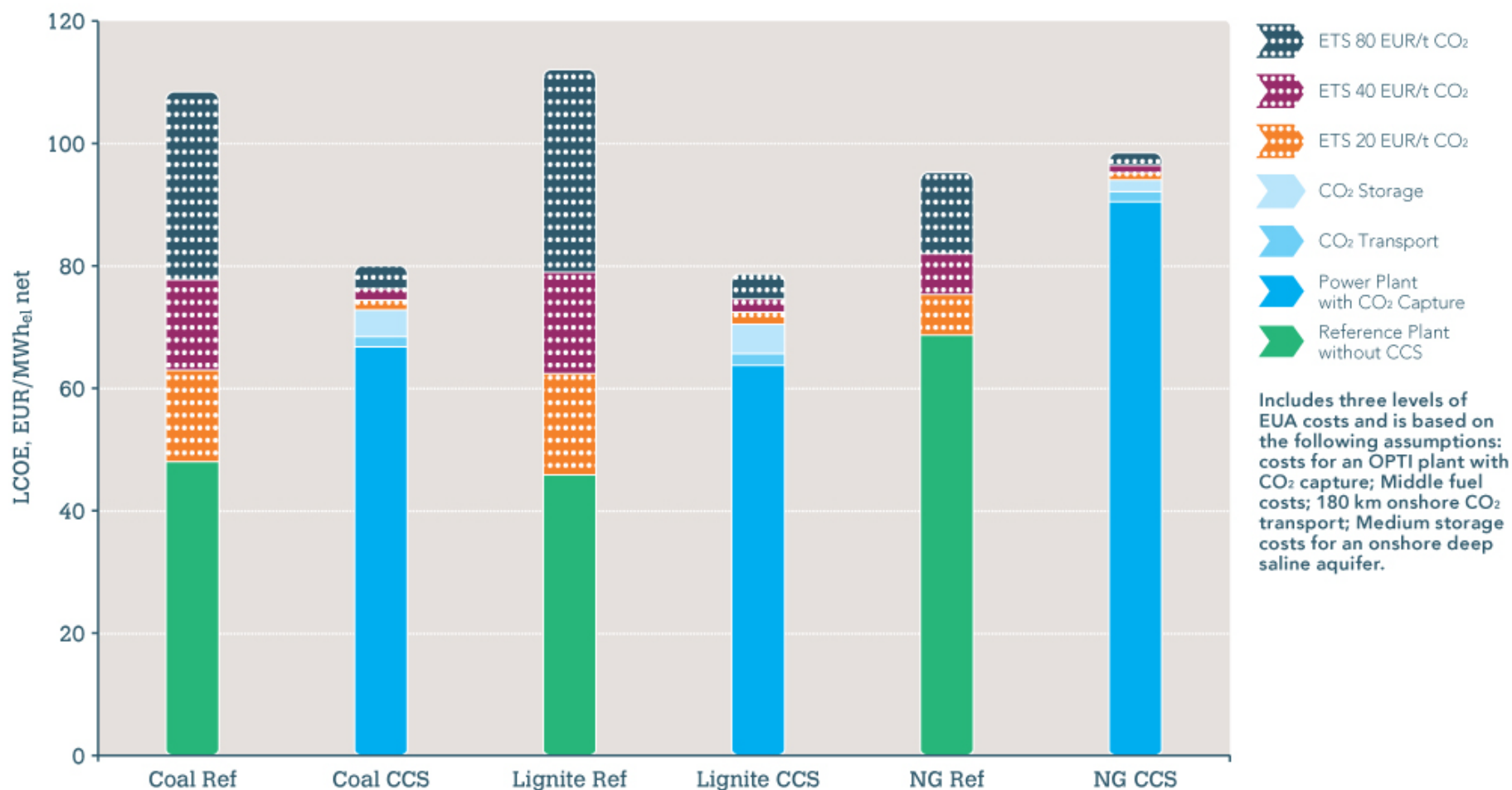
define a strategic agenda for the development and deployment of technologies in the EU involving major economic or societal challenges.

- Initiated by the European Commission in 2005
- **Unique coalition of stakeholders:**  
**European utilities, petroleum companies, equipment suppliers, scientists, academics and environmental NGOs**
- Over 300 members from 19 countries

[www.zeroemissionplatform.eu](http://www.zeroemissionplatform.eu)

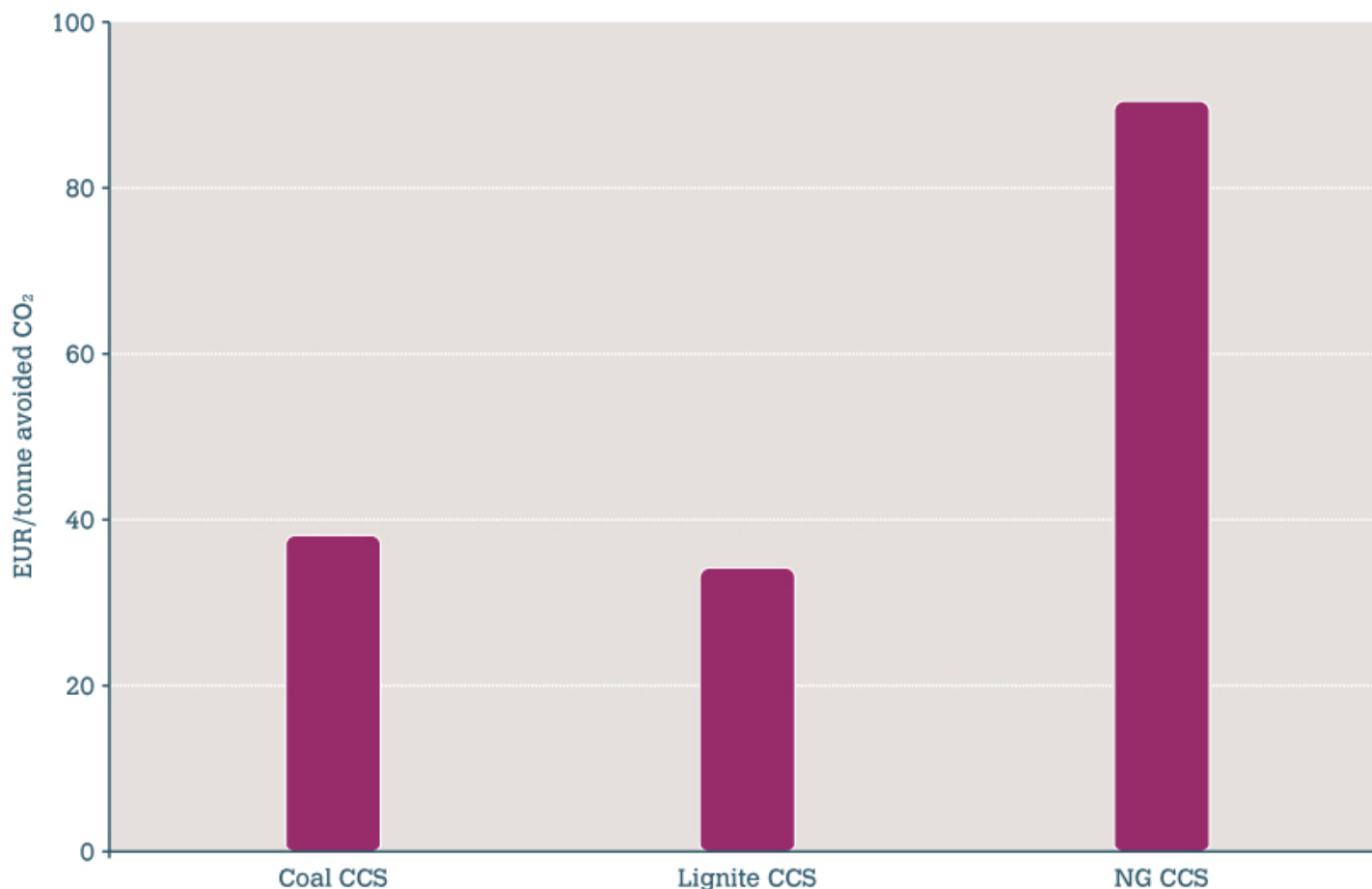
# Levelized Cost of Electricity LCOE for Integrated CCS projects (coal and gas)

Figure 1: The Levelised Cost of Electricity (LCOE) of integrated CCS projects (blue bars) compared to the reference plants without CCS (green bars)



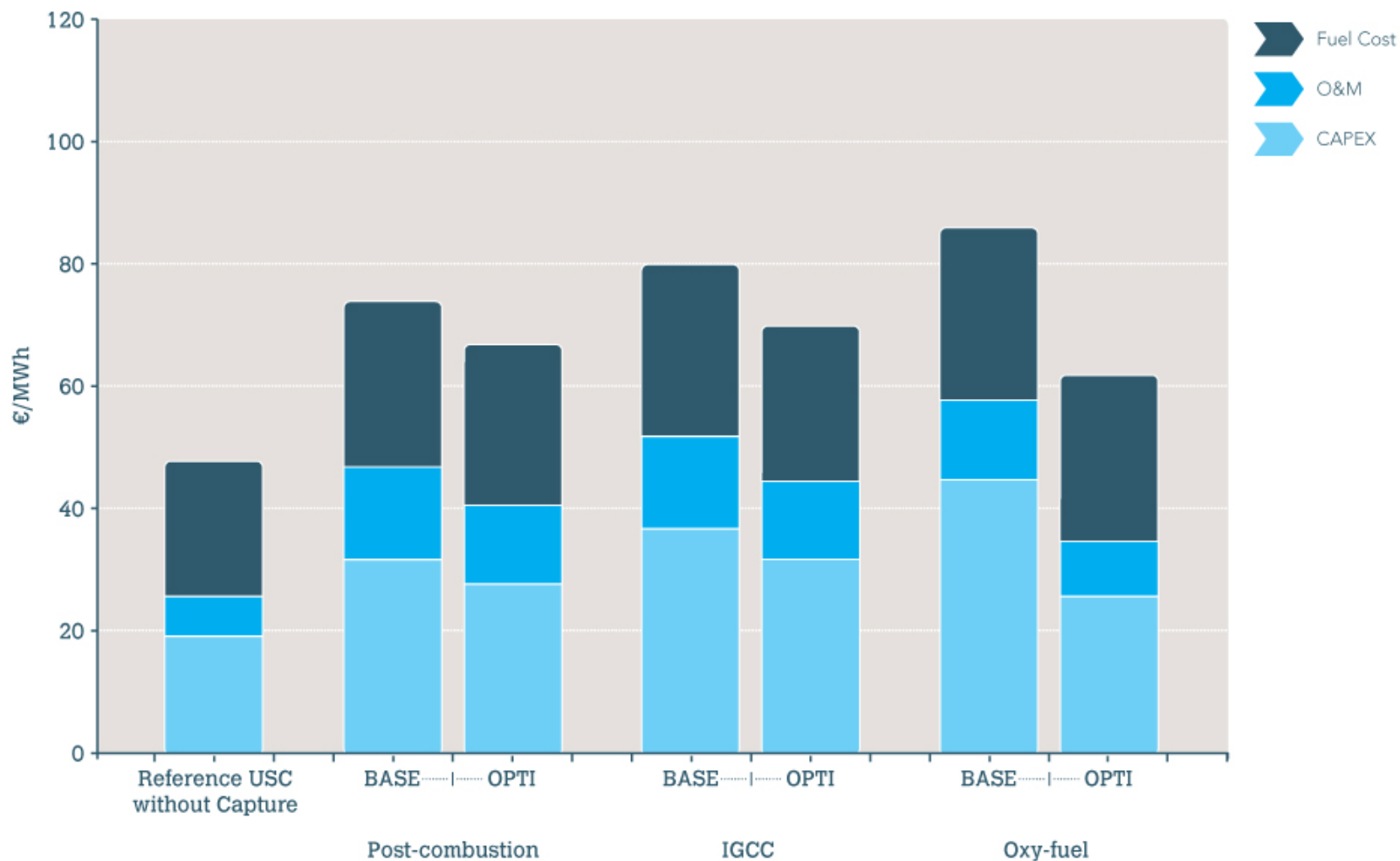
# CO<sub>2</sub> Avoidance Costs – Price of EUAs to Justify Building CCS Projects vs. Plant w/o CCS

Figure 13: CO<sub>2</sub> avoidance costs for possible plants commissioned in the mid 2020s – the price of EUAs required to justify building CCS projects vs. a plant without CCS from a purely economic point of view (calculated on the same basis as Figure 12)



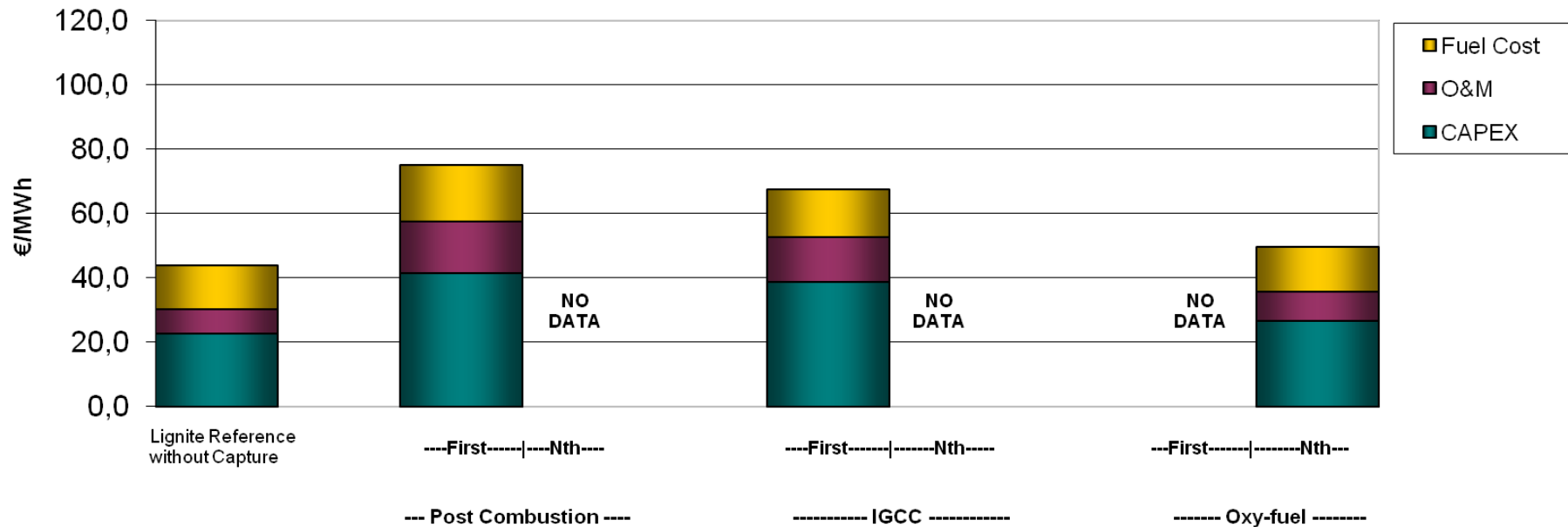
# LCOE for Hard Coal Plants with CO<sub>2</sub> Capture (capture-costs only)

Figure 14: The LCOE for hard coal-fired power plants with CO<sub>2</sub> capture (using Middle fuel costs)

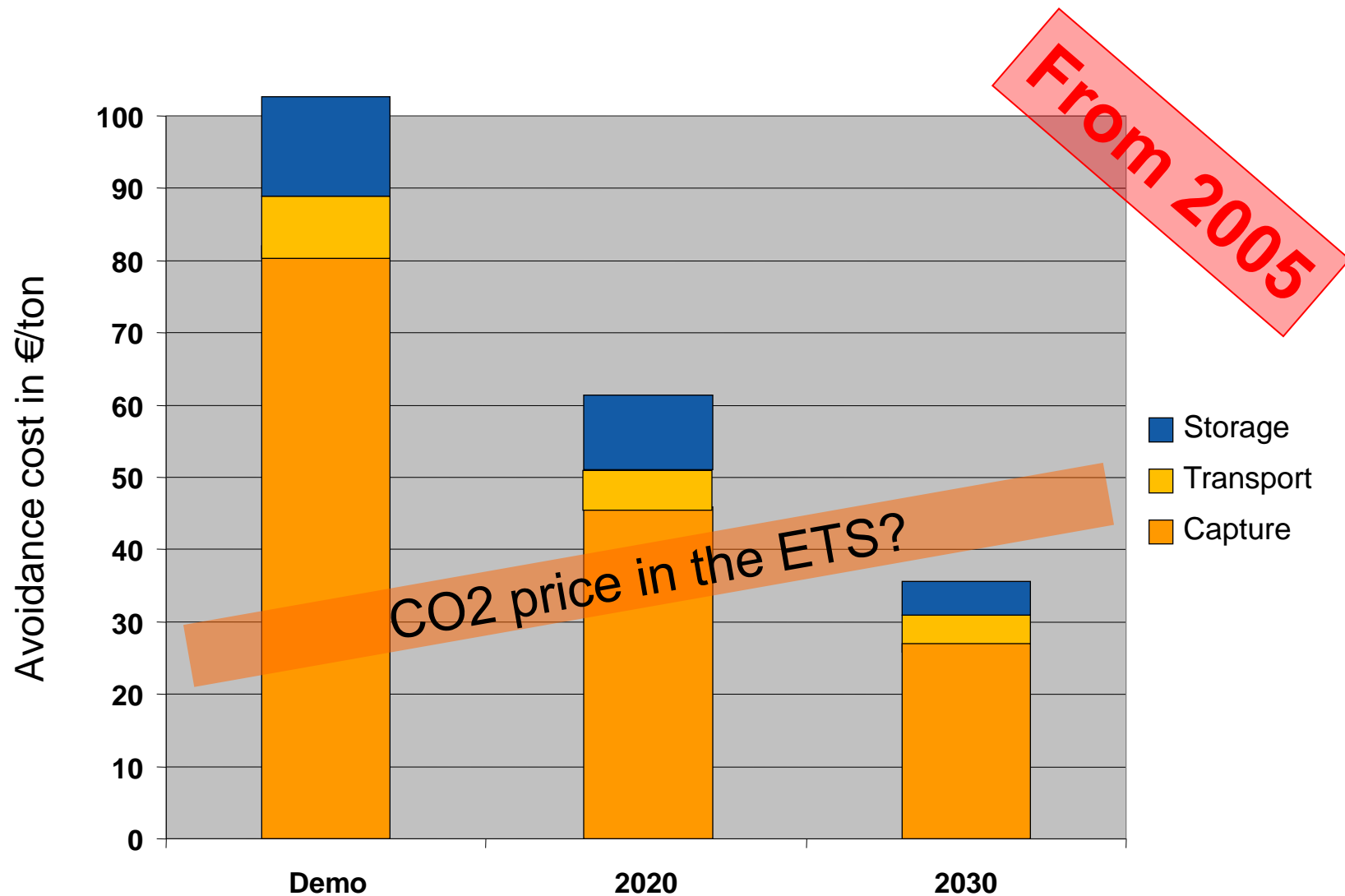




# LCOE for Lignite Plants with CO<sub>2</sub> Capture (capture-costs only)



# Total cost, including transport and storage (€/ton CO<sub>2</sub>)

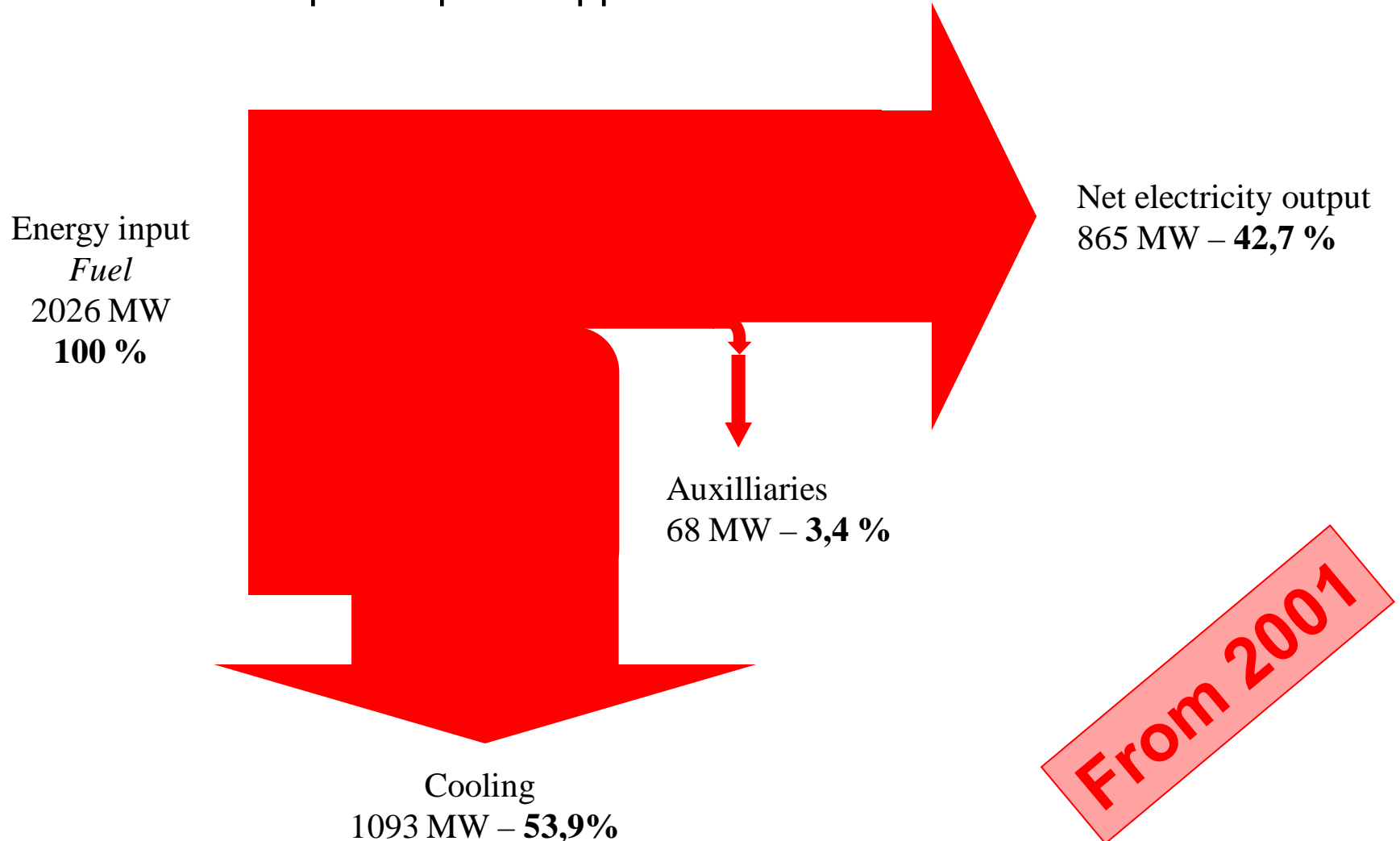


# Power Plant Lippendorf



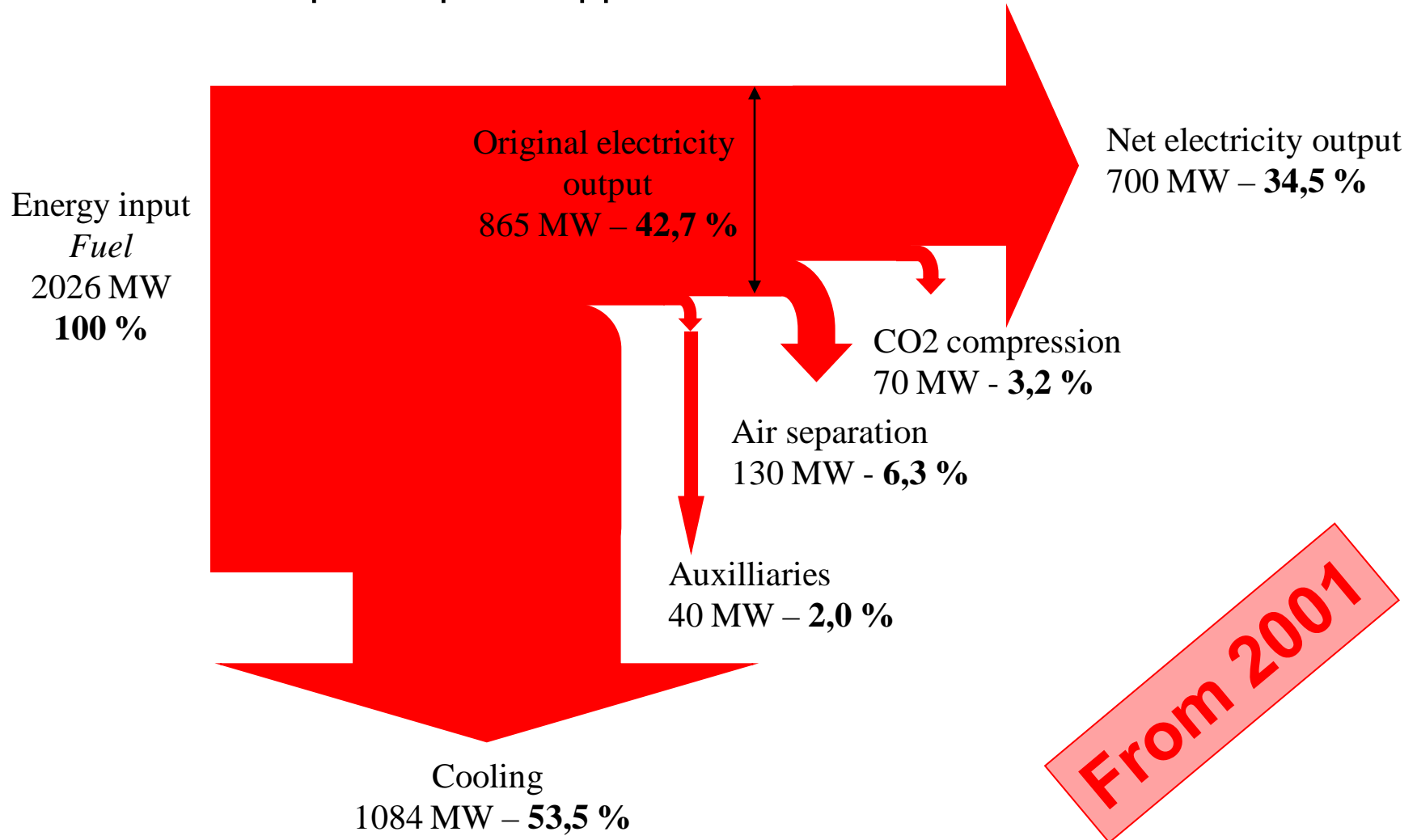
# Energy flow diagram for a lignite fired Power Plant

## Base case power plant Lippendorf



# Energy flow diagram for lignite fired plant with O<sub>2</sub>/CO<sub>2</sub> combustion

## Base case power plant Lippendorf





# Alternative flue gas and CO<sub>2</sub> processing in Schwarze Pumpe



## Characterisation and Evaluation of new technology for CO<sub>2</sub>- processing

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# CCS Demonstration Plant Jämschwalde



# Demonstration Plant Jämschwalde – Technical data

Compare Lippendorf study from 2001

## Oxyfuel:

- Newly build single block at existing power plant site
- Capacity 250 MWe
- Efficiency (net) 36 %
- Separated CO<sub>2</sub> 1,34 Mio.t/a
- Specific CO<sub>2</sub>-emissions 78 g/kWh

## Post combustion capture

- Retrofitting of a part of an existing unit
- Capacity 50 MWe
- Separated CO<sub>2</sub> 0,39 Mio.t/a
- Specific CO<sub>2</sub>-emissions 107 g/kWh





# CO2 Injection Ketzin



- Preparing for injection of CO2 in Ketzin outside Berlin, in cooperation with GFZ Potsdam

# The Oxyfuel Technology progress under full sail



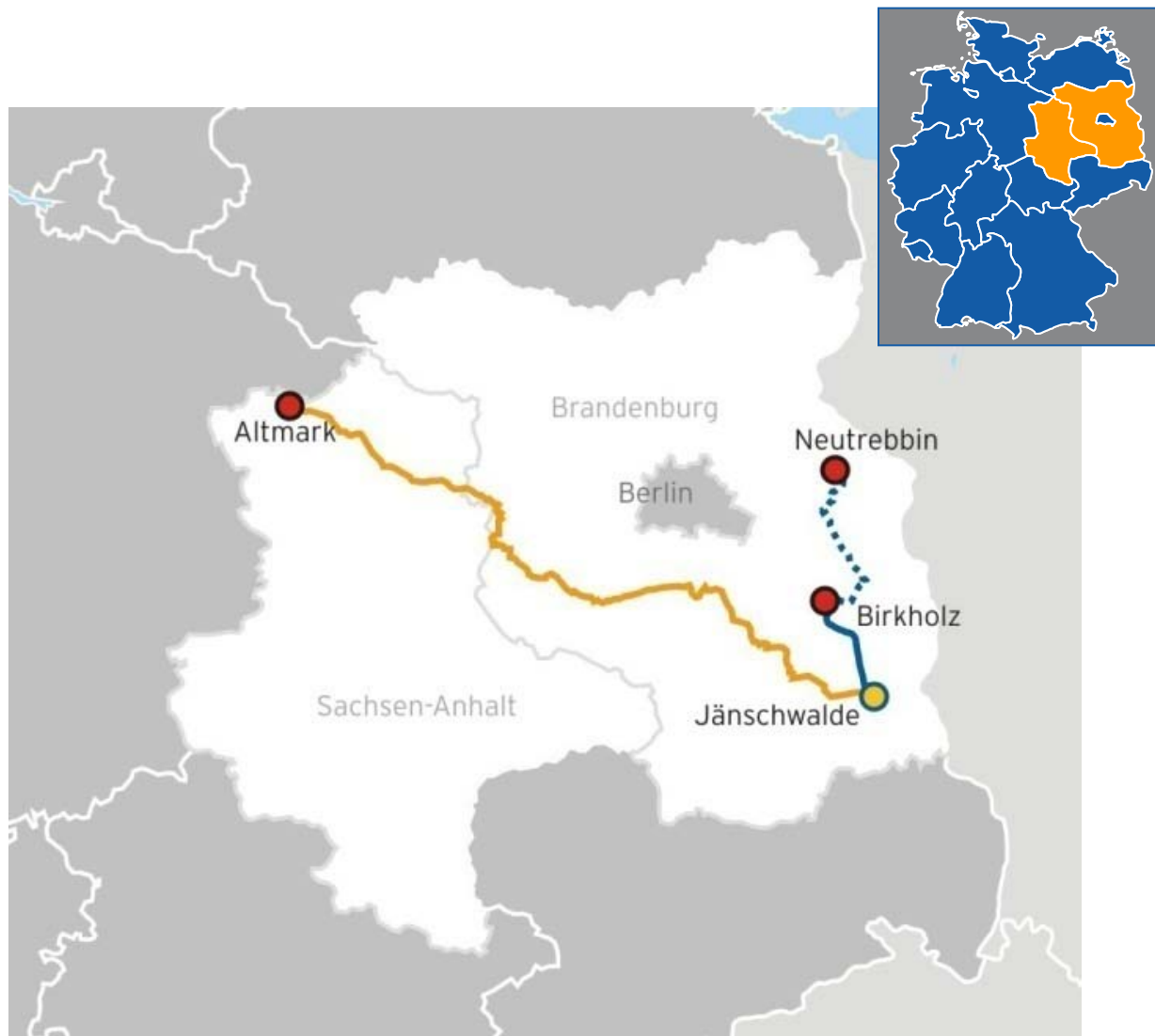
# Demonstration Plant Jänschwalde – Potential storage sites

## I. Brandenburg

Storage in deep saline aquifers  
(pipeline 50/140 km)

## II. Altmark

EGR pilot project in  
cooperation with  
Gaz de France  
(pipeline 300 km)











4-6 vibrator trucks 25 ton  
Distance between vibrations app. 10 m  
Daily capacity app. 7 km  
Manning 60 – 80



# Build trust by communication and transparency

## ➤ **DIREKT contact**

- Public hearings
- Information via local press and brochures
- Telefon-Hotline 0800-1243683
- [www.vattenfall.de/ccs](http://www.vattenfall.de/ccs)

## ➤ **PERSONAL contact**

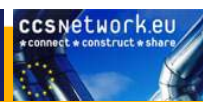
- CCS-Infocenter
- Stakeholder meetings

## ➤ **TRANSPARENT**

- Regional stakeholder committee
- Applications and permissions are public
- On the internet



# And the answer is.....

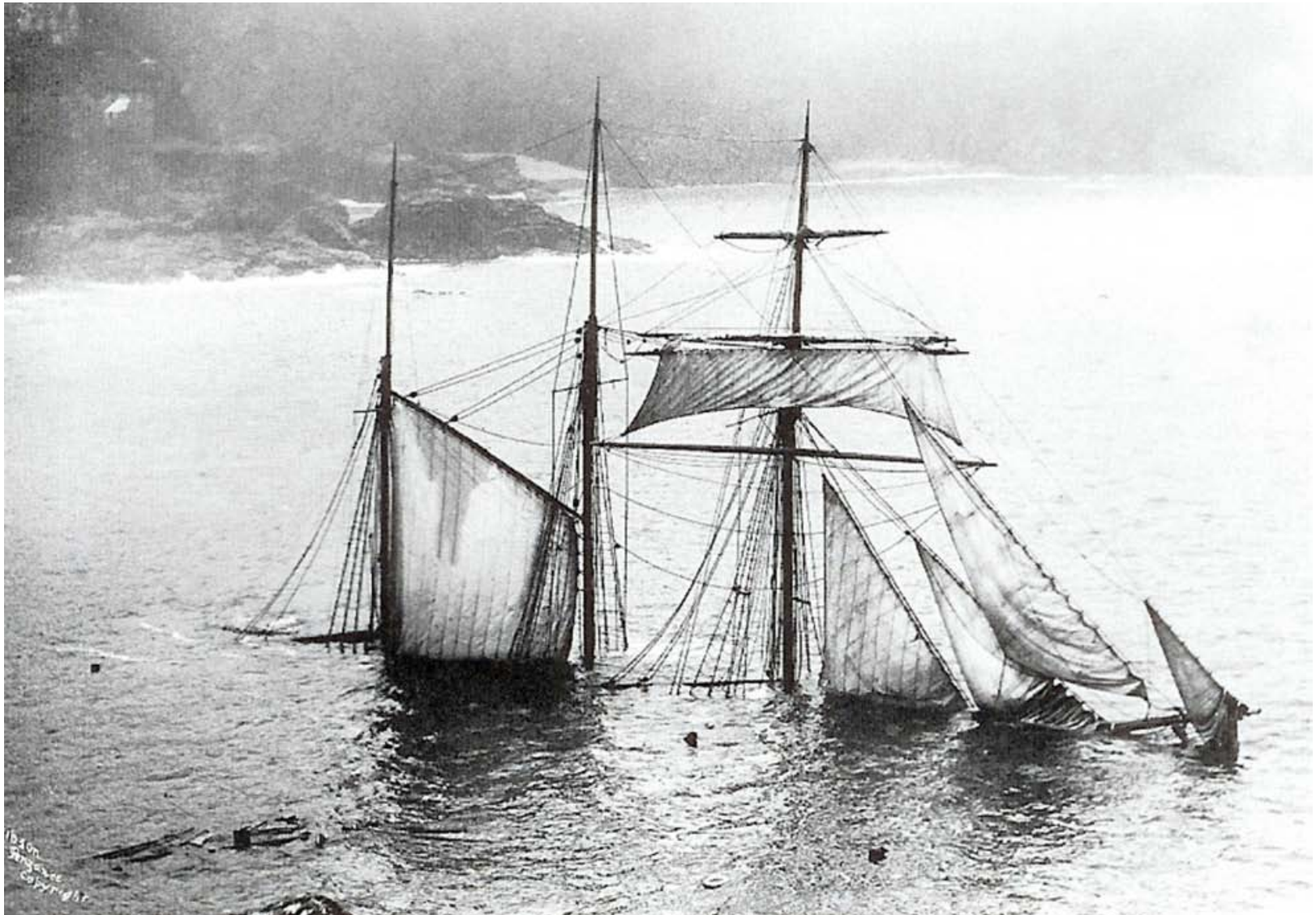


# In Europe we have ran into a blind alley.

- We spend an enormous amount of money on technology development and make very good progress.
  - Own efforts on oxyfuel has progressed very well and we get better experience from our pilot plant than expected
  - We have made large improvement giving lower cost, less energy needed and much better performance.
  - Our demonstration plant is already engineered and designed
  - We are ready to build
- We are effectively stopped everywhere by different parts of the society
  - Regional politicians, implementing the EU law in national legislation effectively killing any attempt to proceed
  - Our colleagues in Denmark, Holland, Germany, Sweden and Italy experience the same
  - Even in Norway they got cold feet when fulfilling promise for transport and storage
- Politicians say we need CCS for several reasons, and we get nowhere at present.



# The European CCS demonstration programme ?



# Oxyfuel Combustion Technology - way forward

- Oxyfuel Combustion Technology is very straightforward.
  - We have shown to anyone that it is a simple way forward
  - The process works and it works well
  - The new components as ASU, CPU are easy to incorporate in a power plant, and they work well
  - The traditional components as boilers, ESP, FGD and flue gas condensing unit are well suited also for oxyfuel combustion
- The combustion process is actually easier to handle, since we have another operational factor to utilize, the O<sub>2</sub> content.
- The rest products as gypsum and ash are just as good as for conventional processes
- It seems product development will get us as close to “zero emissions” to the atmosphere as is possible
- The CO<sub>2</sub> product can be delivered at any desired quality.
- The economy seems superior to competing technologies.



Give us a chance to build a full size unit somewhere !



# CCS Demo Plant, Jämschwalde unit G



# Back – up ?

